

CLAIMS

The embodiment of the invention in which an exclusive property or privilege is claimed is defined as follows:

- 1        1. A process for rapidly heating a fuel processor to its operating  
2 temperature, the process comprising:
  - 3        a) reforming fuel with a catalyst to produce steam, carbon monoxide, and hydrogen  
4 gas;
  - 5        b) homogeneously mixing air with the carbon monoxide and hydrogen gas to create  
6 a mixture which will react and produce heat;
  - 7        c) using the heat to raise the temperature of catalysts in the fuel processor;
  - 8        d) combining the mixture with an oxidant to decrease the concentration of carbon  
9 monoxide;
  - 10      e) using the heat to produce steam; and
  - 11      f) mixing the steam with the mixture to increase the yield of hydrogen gas.
- 1        2. The process as recited in claim 1 wherein a front edge of the reforming  
2 catalyst is heated to a temperature at which a fuel-air mixture ignites and generates  
3 heat which can be used for vaporization of subsequent fuel.

1           3.       The process as recited in claim 1 wherein the catalyst causes catalytic  
2       partial oxidation (CPOX).

1           4.       The process as recited in claim 3 wherein the partial oxidation is of  
2       hydrocarbons with oxygen (O<sub>2</sub>) to produce carbon monoxide (CO), hydrogen (H<sub>2</sub>),  
3       carbon dioxide (CO<sub>2</sub>), and water (H<sub>2</sub>O).

1           5.       The process as recited in claim 1 wherein the mixture is subjected to  
2       catalyst at a temperature of from about 25<sup>0</sup>C to 500<sup>0</sup>C.

1           6.       The process as recited in claim 1 wherein the oxidizing agent facilitates  
2       the oxidation of hydrogen and carbon monoxide.

1           7.       The process as recited in claim 1 wherein the air-carbon monoxide-  
2       hydrogen gas mixture contains an oxygen/carbon ratio of more than one and less than  
3       2.

1           8.       The process as recited in claim 1 wherein the fuel can be liquid, vapor, or  
2       a combination thereof.

1           9.       The process as recited in claim 5 wherein the temperature is reached  
2       within 30 seconds.

1           10.      The process as recited in claim 1 wherein the air-to-fuel and steam-to-fuel  
2       ratios are adjusted to have temperatures in the reforming fuel catalyst from between  
3       about 600<sup>0</sup>C to 850<sup>0</sup>C.

1           11.      The process as recited in claim 1 wherein the maximum temperature in  
2       the reforming fuel catalyst is about 900<sup>0</sup>C.

1       12.     A method for converting hydrocarbon fuels to a reformate gas, the  
2     method comprising:

3     a)    producing combustible moieties from the fuels;  
4     b)    oxidizing the combustible moieties to generate heat;  
5     c)    utilizing the heat to increase the surface temperatures of catalysts; and  
6     d)    contacting the reactants to the catalysts.

1       13.     The method as recited in claim 12 wherein the step of producing  
2     combustible moieties further comprises combining the fuel with an oxidant to create a  
3     mixture.

1       14.     The method as recited in claim 13 wherein the oxygen/carbon ratio of the  
2     mixture is more than one and less than 2.

1       15.     The method as recited in claim 12 wherein the combustible moieties are  
2     carbon monoxide and hydrogen.

1       16.     The method as recited in claim 12 wherein the step of contacting the fuel  
2     to the catalyst results in the formation of carbon monoxide and hydrogen gas.

1       17.     The method as recited in claim 15 wherein a portion of the carbon  
2     monoxide and hydrogen is reacted with oxygen to create heat.

1       18.     The method as recited in claim 17 wherein the heat raises the  
2     temperature of a water-gas shift catalyst so the catalyst becomes active for its water-  
3     gas shift reaction which converts carbon monoxide and generates additional heat.

1       19.     The method as recited in claim 12 wherein air is injected downstream of  
2     the catalysts to have complete oxidation of all combustible moieties before  
3     the combustible moieties have egress from the system.

1           20.       The method as recited in claim 12 wherein liquid water is injected when  
2       the water-gas shift catalyst temperature exceeds 400°C.

1           21.       The method as recited in claim 19 wherein the liquid water is injected in  
2       the form of water droplets having diameters less than 50 microns ( $\mu$ ).

1           22.       A device for the vaporization of fuel, the device comprising:  
2           a) a means to provide the latent heat of vaporization of the fuel; and  
3           b) a means to provide superheating of the fuel.

1           23.       The device as recited in claim 22 wherein the means to provide the  
2       latent heat of vaporization of the fuel is a first heating element.

1           24.       The device as recited in claim 22 wherein the means to provide  
2       superheating of the fuel is a second heating element.